

## THE PHOTOLYSIS OF GASEOUS NITROUS ACID

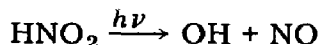
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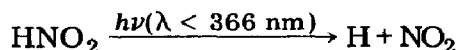
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### Summary

The photolysis at 330 - 380 nm of mixtures containing parts per million concentrations of gaseous nitrous acid in pure nitrogen and oxygen has been studied in a flow system. The rates of formation of the products NO and NO<sub>2</sub>, have been measured at low conversion of HNO<sub>2</sub>. From these data it has been shown that the predominant process following absorption by HNO<sub>2</sub> in this wavelength region is the dissociation

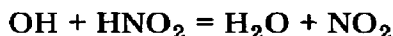


There is some evidence for the occurrence of the alternative process:



which may account for ~ 10% of the overall photodissociation.

An estimate of the rate constant for the reaction



has also been obtained. The value,  $k_3 = 1.8 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ sec}^{-1}$  (based on a literature value for the rate constant for the reaction of OH with NO<sub>2</sub>), is about one order of magnitude higher than for the analogous reaction of OH with HNO<sub>3</sub>.

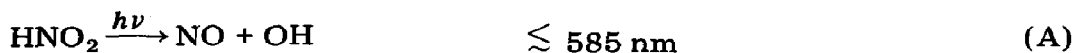
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### Introduction

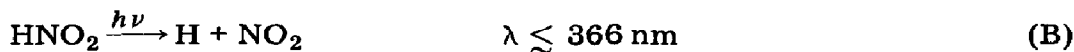
Nitrous acid has been postulated as an intermediate in many gas-phase reactions involving the oxides of nitrogen and hydrogen containing compounds. However, there is very little experimental information regarding the chemical and photochemical behaviour of gaseous nitrous acid. This results mainly from the practical difficulty in obtaining reasonable concentrations of gaseous HNO<sub>2</sub> because of the rapid establishment of the equilibrium (I) at pressures of a few Torr [1]:



We have recently reported a method for the preparation and quantitative analysis of mixtures containing low concentrations of gaseous nitrous acid in air at 1 atm. ( $\approx 101.33 \text{ kN/m}^2$ ) pressure [2]. Although both NO and NO<sub>2</sub> were unavoidably present, stable concentrations of HNO<sub>2</sub> greatly in excess of those predicted by the equilibrium (I) could be obtained. This has facilitated, for the first time, systematic studies of the photolysis of gaseous nitrous acid. The results of a preliminary investigation on this system have already been reported [3]. It was found that the products of the steady-state photolysis of HNO<sub>2</sub> at  $\lambda = 365 \text{ nm}$  are NO, NO<sub>2</sub> and probably HNO<sub>3</sub>. The kinetics of the reactions following photolysis were complex and could not be adequately described by the following simple mechanism which was based on available spectroscopic, thermodynamic and kinetic information:



In particular, the yield of NO was much less than expected and it was suggested that this may be due to the occurrence of the alternative dissociation process:



There are, however, other possible explanations of the observed behaviour, and it seemed desirable to establish with more certainty the nature of the primary photodissociation process(es) in the photolysis of HNO<sub>2</sub>.

The present paper describes a study of the photolysis (at 330 - 380 nm) of dilute mixtures containing predominantly nitrous acid in pure nitrogen and oxygen, in a flow system, using short irradiation periods. The rates of formation of the products NO and NO<sub>2</sub> have been determined at HNO<sub>2</sub> conversions of approximately 3%. From these data it has been shown that the predominant ( $\sim 90\%$ ) primary dissociation process yields hydroxyl radicals and nitric oxide with a possible small contribution from process (B). Estimates of the quantum yield for dissociation and of the rate constant for the reaction of OH with HNO<sub>2</sub> have also been made.

## Experimental

The photolyses were carried out in a 27 cm<sup>3</sup> cylindrical Pyrex cell, 7 cm in length and 2.2 cm diameter, with planar quartz end windows cemented on with Araldite. The cell was mounted in an optical system comprising a

high pressure mercury arc lamp (Mazda type ME/D, 250 W), two quartz lenses ( $f = 5$  cm), glass filters (4 mm Pyrex + Chance OX1) and an adjustable stop. The system was arranged to give a slightly convergent beam through the cell. The waveband isolated by the filters was 330 - 380 nm and approximately 50% of the radiation entering the cell was at  $365 \pm 5$  nm. The wavelength region utilized corresponds to the principal absorbing region for gaseous nitrous acid in its first absorption band [4].

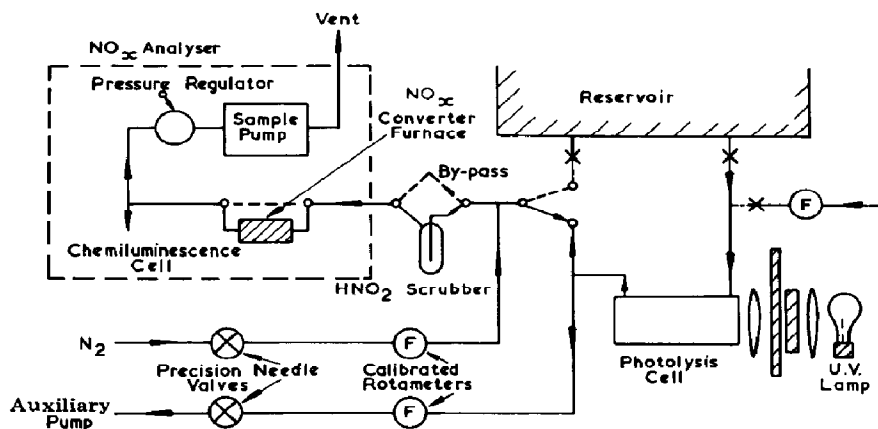


Fig. 1. Diagram of flow apparatus.

A diagram of the flow system used for the photolysis measurements is shown in Fig. 1. Entry and exit tubes to the cell were positioned close to the front and rear windows. Gas mixtures were drawn through the cell from a 250 l bag constructed of Tedlar film (du Pont Ltd). The flexible bag, which was shielded from room light provided a convenient, constant pressure (1 atm.) reservoir for the gas mixtures. The gas flow was provided by a combination of the analyzer sample pump and an auxiliary diaphragm pump (Charles Austin, Capex Mk II). The analyzer drew a constant flow of  $10 \text{ cm}^3/\text{s}$  at 1 atm. When a faster flow was required, additional gas was metered through the system by means of the auxiliary pump. If the gas flow to the analyzer exceeded the required flow through the cell, pure nitrogen was metered into the gas stream, downstream from the cell. The total flow through the reaction vessel could be measured directly at the cell inlet prior to taking measurements. It was assumed that the flow rates used ( $1 - 20 \text{ cm}^3/\text{s}$ ) gave sufficient turbulence for the gases to be completely mixed within the cell. The photolyses were carried out at atmospheric pressure and at room temperature ( $300 \pm 2 \text{ K}$ ). All gas lines were of  $1/8$  in. (1 in. = 25.4 mm). Teflon tubing to minimize adsorption loss of the oxides and oxyacids of nitrogen.

Analysis of the nitrogen gases was carried out with a commercial chemiluminescence " $\text{NO}_x$ " analyzer (Thermo-Electron Corp. Model 12A) using the same techniques as described previously [2]. The instrument can measure directly both NO and " $\text{total NO}_x$ " *i.e.*  $\text{NO} + \text{NO}_2 + \text{HNO}_2$ , in a gaseous sample.

Gaseous  $\text{HNO}_2$  can be quantitatively removed from the sample gas by absorption in aqueous 0.1 *N* NaOH contained in a miniature scrubber. Thus the concentrations of all three components can be determined after allowance for the small but constant fraction ( $12.5 \pm 0.5\%$ ) of the  $\text{NO}_2$  which is also absorbed in the alkali. Samples to the analyzer could be taken either directly from the reservoir or downstream of the photolysis cell.

In order to prepare mixtures of gaseous nitrous acid the reservoir was first flushed with  $\text{N}_2$  and pumped out with a high volume rotary blower. 90 l  $\text{O}_2$  were then admitted to the bag. Dilute  $\text{HNO}_2$  was added by passing  $\text{N}_2$  at  $167 \text{ cm}^3/\text{s}$  through a 100 ml flask containing  $\sim 35 \text{ ml}$  0.02 *M* sodium nitrite acidified to  $\text{pH} = 0$  with  $\text{H}_2\text{SO}_4$ . The gases passed into the reservoir through a short length of PTFE tubing. The glass surfaces of the flask were coated with PTFE and the glassware was oven dried before use. With this procedure approximately 85% of the "nitrous fumes" swept into the reservoir was gaseous  $\text{HNO}_2$ , the balance being  $\text{NO}$  and  $\text{NO}_2$  in roughly equal proportions. After sufficient  $\text{HNO}_2$  had been added, the reservoir was filled to 250 l with  $\text{N}_2$ . Mixtures containing up to 20 ppm  $\text{HNO}_2$  ( $1 \text{ ppm} = 2.46 \times 10^{13}$  molecules/ $\text{cm}^3$  at 300 K and 1 atm. pressure) were prepared in this way and were found to undergo little change in composition on standing for several hours in the reservoir.

The rate of photolysis of  $\text{HNO}_2$  was measured from the change of composition of the gas mixture when it was passed through the photolysis cell at a given flow rate. First, it was necessary to examine any changes in composition resulting from passage of the mixture through the unirradiated cell. An extensive series of tests showed that there was no detectable change in the concentrations of  $\text{NO}$  and  $\text{NO}_2$  when  $\text{HNO}_2$ - $\text{NO}$ - $\text{NO}_2$  mixtures were passed through the cell (without irradiation). There was a small loss in  $\text{HNO}_2$  which was more pronounced at the lower  $\text{HNO}_2$  concentrations and at the slower flow rates used. The maximum loss for the conditions employed for rate measurements was 4% and it was normally less than 1%.

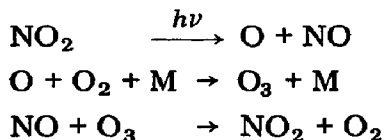
Since the concentrations of  $\text{NO}$  and  $\text{NO}_2$  were unaffected by passage through the unirradiated cell, the rate of formation,  $R_f$ , of these components during photolysis could be determined from the change in concentration of  $\text{NO}$  and  $\text{NO}_2$  in the cell effluent resulting from irradiation of the mixture, *i.e.*

$$R_f = \frac{F}{V} \times \Delta C$$

where  $F$  = volumetric flow rate ( $\text{cm}^3/\text{s}$ ),  $V$  = volume of the cell ( $27 \text{ cm}^3$ ) and  $\Delta C$  = change in concentration. In a typical experiment the following procedure was adopted: the concentrations of  $\text{HNO}_2$ ,  $\text{NO}$  and  $\text{NO}_2$  in the reservoir were measured and the gas mixture was drawn through the photolysis cell at the required flow rate until a constant "total  $\text{NO}_x$ " reading was obtained in the effluent. A series of measurements of the effluent  $\text{NO}$  and " $\text{NO} + \text{NO}_2$ " (*i.e.* sampling through the scrubber) were taken with and without irradiation and the average differences  $\Delta C_{\text{NO}}$  and  $\Delta C_{\text{NO}+\text{NO}_2}$  determined. Finally a check

on "total  $\text{NO}_x$ " was made and any change noted.

A complicating feature in the irradiation of these mixtures arises from the photolysis of  $\text{NO}_2$ .  $\text{NO}_2$  absorbs throughout the wavelength region employed and, at low  $[\text{NO}_2]$ , produces NO by the reactions:



At the light intensity and the photolysis times used the net change in NO and  $\text{NO}_2$  concentration from these reactions was not negligible. Therefore, in order to determine the rates of formation of NO and  $\text{NO}_2$  ( $R_{\text{NO}_2}$ ) in the photolysis of  $\text{HNO}_2$  it was necessary to correct the observed  $\Delta C$  values for the changes produced by the photolysis of  $\text{NO}_2$ . This was achieved by independent measurements taken when mixtures containing NO and  $\text{NO}_2$  but no  $\text{HNO}_2$  were photolyzed. The  $\text{HNO}_2$  was removed by passage of the gas mixture through the alkali scrubber prior to entering the photolysis cell. The NO and  $\text{NO}_2$  concentrations were then close to those present in the original mixture and the  $\Delta C_{\text{NO}}$  values, determined at the appropriate flow rate were used to correct the observed changes in NO and "NO +  $\text{NO}_2$ " for the  $\text{HNO}_2$ -NO- $\text{NO}_2$  mixture,\* *i.e.*

$$R_{\text{NO}} = \frac{F}{V} [\Delta C_{\text{NO}} - (\Delta C_{\text{NO}})_{\text{NO}_2}]$$

$$R_{\text{NO}_2} = \frac{F}{V} \Delta C_{\text{NO}+\text{NO}_2} - R_{\text{NO}}$$

For mixtures containing predominantly  $\text{HNO}_2$ , the correction  $(\Delta C_{\text{NO}})_{\text{NO}_2}$  was between 5 and 37% of the total  $\Delta C_{\text{NO}}$ . Thus the photolysis of  $\text{NO}_2$  contributed a sizeable fraction of the total NO production and hence reduced the accuracy with which  $R_{\text{NO}}$  and  $R_{\text{NO}_2}$  could be determined. In a typical experiment  $\Delta C_{\text{NO}}$  and  $\Delta C_{\text{NO}+\text{NO}_2}$  were approximately 15 and 20% of the initial NO and NO+ $\text{NO}_2$  concentrations respectively. The reproducibility of a measured concentration was to within 1% and therefore the  $\Delta C$  values had an estimated error of  $\pm 3\%$ . After correction for  $(\Delta C_{\text{NO}})_{\text{NO}_2}$  (which typically had an error of  $\pm 10\%$ ), the estimated errors in single determinations of  $R_{\text{NO}}$  and  $R_{\text{NO}_2}$  were  $\pm 6$  and  $\pm 7.5\%$  respectively. The errors were proportionally larger at higher relative NO and  $\text{NO}_2$  concentrations but the uncertainty could be reduced by repeated measurements on a given mixture.

In order to check that the concentration changes produced by photolysis were representative of the initial rates of product formation, a series of tests were carried out in which the  $\Delta C$  values were determined at different

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\*There was, as expected, no measurable change in the total NO +  $\text{NO}_2$  when mixtures of NO and  $\text{NO}_2$  were photolyzed.

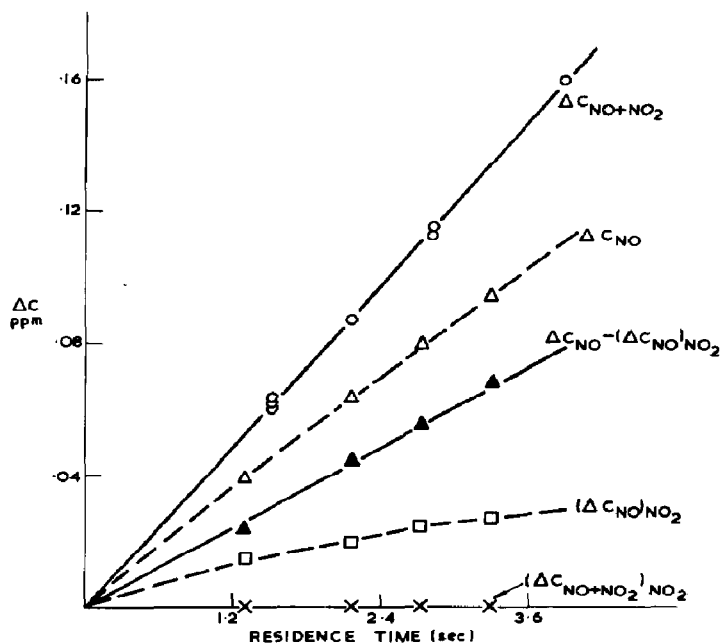


Fig. 2. Effect of reactor residence time on the observed concentration changes in the photolysis of  $\text{HNO}_2\text{-NO-NO}_2$  and  $\text{NO-NO}_2$  mixtures. Initial concentrations in the two mixtures were  $\text{HNO}_2 = 3.24$  ppm,  $\text{NO} = 0.56$  ppm,  $\text{NO}_2 = 0.44$  ppm, and  $\text{NO} = 0.56$  ppm,  $\text{NO}_2 = 0.39$  ppm respectively.  $\circ, \Delta$  = measurements made on mixture containing  $\text{HNO}_2$ ;  $\times, \square$  = measurements made on mixture containing only  $\text{NO} + \text{NO}_2$ . Filled triangles show formation of  $\text{NO}$  from  $\text{HNO}_2$  photolysis.

flow rates through the photolysis cell. Figure 2 shows  $\Delta C_{\text{NO}}$ ,  $\Delta C_{\text{NO}+\text{NO}_2}$ ,  $(\Delta C_{\text{NO}})_{\text{NO}_2}$  and  $[\Delta C_{\text{NO}} - (\Delta C_{\text{NO}})_{\text{NO}_2}]$  plotted against reactor residence time,  $\tau$ , for the photolysis of a mixture containing initially 3.24 ppm  $\text{HNO}_2$ , 0.56 ppm  $\text{NO}$  and 0.44 ppm  $\text{NO}_2$ . It will be seen that although the production of  $\text{NO}$  from  $\text{NO}_2$  was non-linear the values of  $\Delta C_{\text{NO}+\text{NO}_2}$  and  $\Delta C_{\text{NO}} - (\Delta C_{\text{NO}})_{\text{NO}_2}$  increased linearly up to  $\tau \simeq 3$  s. For most rate determinations standard flow conditions giving  $\tau = 2.2$  s were employed.

The incident light intensity in the cell was estimated from measurement of the rate of photolysis of  $\text{NO}_2$  (18 ppm) in 1 atm.  $\text{N}_2$ . The specific absorption rate ( $k'_a$ ) for  $\text{NO}_2$ , derived from the rate of  $\text{NO}_2$  photolysis, was  $2.8 \times 10^{-2} \text{ s}^{-1}$  which corresponds to a photon flux of  $5.4 \times 10^{16}$  quanta/s. However, subsequent checks showed that the lamp output varied considerably (up to 30%) from day to day and, since the light intensity was not monitored during the experiments, a correction for these variations could not be made. Short term fluctuations in intensity were much less ( $< 3\%$  per hour).

Oxygen (breathing grade;  $> 99.5\%$   $\text{O}_2$ ,  $\sim 0.5\%$   $\text{Ar}$ ; 20 ppm  $\text{C}$  (mainly  $\text{CO}_2$  and  $\text{CH}_4$ ),  $\text{CO} = \text{nil}$ ) and nitrogen (oxygen free grade,  $\text{CO} = \text{nil}$ ,  $\text{CO}_2 < 5$  ppm, hydrocarbon  $< 5$  ppm) were taken directly from cylinders. Nitric oxide was obtained from a cylinder containing a mixture of  $\text{NO}$  (130 ppm) in nitrogen. The sodium nitrite, sodium hydroxide and water were Analar grade.

TABLE 1

Rates of formation of NO and NO<sub>2</sub> in the photolysis of gaseous HNO<sub>2</sub>

Initial concentrations (ppm)			Formation rates (ppm s <sup>-1</sup> × 10 <sup>2</sup> )	
HNO <sub>2</sub>	NO	NO <sub>2</sub>	R <sub>NO</sub>	R <sub>NO<sub>2</sub></sub>
18.33	1.96	2.31	10.22	12.20
16.05	1.96	3.39	9.75	8.10
9.13	0.873	0.542	5.81	6.12
9.00	1.54	1.16	6.23	4.43
8.86	0.608	0.900	6.58	4.73*
8.46	1.53	1.26	5.41	3.77
8.18	0.390	1.33	5.98	4.93*
3.24	0.595	0.461	1.98	2.17
2.76	0.101	0.582	2.05	1.42*
2.64	0.557	0.463	1.32	1.60
2.00	0.214	0.156	1.14	1.46
1.29	0.183	0.113	0.653	0.775
1.06	0.090	0.102	0.608	0.686
0.98	0.102	0.095	0.593	0.636
0.87	0.102	0.100	0.435	0.556
1.31	0.124	0.116	0.698	0.833
1.29	0.183	0.113	0.616	0.775†
1.25	0.272	0.111	0.476	0.715†
1.19	0.440	0.110	0.360	0.650†
0.835	0.078	0.060	0.428	0.571
0.807	0.180	0.058	0.295	0.551†
0.793	0.330	0.055	0.215	0.410†
0.775	0.971	0.054	0.041	0.321†

\*Runs with [NO]/[NO<sub>2</sub>] reduced by the addition of ozone to the original mixture.

†Runs with additional NO.

## Results and Discussion

Table 1 shows a summary of the rates of formation of NO and NO<sub>2</sub> in the photolysis of mixtures containing initially between 0.8 and 18.5 ppm HNO<sub>2</sub>. The concentrations of HNO<sub>2</sub>, NO and NO<sub>2</sub> are mean values of the measured concentrations at the inlet and outlet of the photolysis cell. The maximum conversion of HNO<sub>2</sub> was approximately 3% and therefore the concentrations are close to those present initially. The  $R_{NO}$  and  $R_{NO_2}$  values are averages of at least three determinations for each mixture, corrected for the NO formation by photolysis of NO<sub>2</sub>.

Most experiments were carried out with an initial HNO<sub>2</sub> concentration of approximately 80 - 85% of the "total NO<sub>x</sub>", the remainder being NO and NO<sub>2</sub>. In a few of these runs (marked \*) the NO/NO<sub>2</sub> ratio was reduced by the addition of a little ozone to the reservoir. The last eight rows in Table 1 show the results for experiments in which increasing amounts of NO were ad-

ded to mixtures containing approximately constant concentrations of  $\text{HNO}_2$  and  $\text{NO}_2$ .

It will be seen from Table 1 that both  $\text{NO}$  and  $\text{NO}_2$  are formed at comparable rates in the photolysis of  $\text{HNO}_2$  and the experiments with added  $\text{NO}$  show clearly that the photolysis is inhibited by  $\text{NO}$ . These observations are qualitatively consistent with the simple photolysis mechanism, comprising the following reactions:



However, this mechanism requires that  $R_{\text{NO}} > R_{\text{NO}_2}$  for all conditions except  $[\text{NO}_2] = 0$  when  $R_{\text{NO}} = R_{\text{NO}_2}$ . This is inconsistent with the data in Table 1 where it will be seen that there was a tendency for  $R_{\text{NO}_2}$  to be greater than  $R_{\text{NO}}$ , particularly in experiments with added  $\text{NO}$  when the difference  $R_{\text{NO}_2} - R_{\text{NO}}$  was far too large to be attributed to experimental error.

There are several possible explanations of the "excess"  $\text{NO}_2$  formation. For example, if a fraction of the  $\text{OH}$  radicals produced in reaction (A) react with a fourth component to yield  $\text{H}$  or  $\text{HO}_2$ ,  $\text{NO}_2$  could be formed in the reaction:



This seems unlikely, however, since the rates of reactions (1) - (3) at pressures near 1 atm. are very rapid ( $k \lesssim 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ ) and impurity gases which can react with  $\text{OH}$  to give  $\text{HO}_2$  (e.g.  $\text{H}_2$ ,  $\text{CO}$ ,  $\text{CH}_4$ ) were not present in the diluent  $\text{N}_2$  and  $\text{O}_2$  at sufficient concentration to compete for  $\text{OH}$  under the experimental conditions. Alternatively,  $\text{NO}_2$  may be produced in a reaction of  $\text{HNO}_2$  with active species produced in the photolysis of  $\text{NO}_2$  [i.e.  $\text{O}(^3\text{P})$ ,  $\text{O}_3$ ] e.g.



At the  $\text{NO}_2$  concentrations employed (up to 3 ppm) the maximum steady-state concentration of  $\text{O}(^3\text{P})$  (resulting from the photolysis of  $\text{NO}_2$ ) was  $\sim 5 \times 10^7 \text{ molecules/cm}^3$ . For reaction (5) to account for 10% of the  $\text{HNO}_2$  removal, the quantity  $k_5[\text{O}]$  is required to be  $8 \times 10^{-4} \text{ s}^{-1}$  i.e.  $k_5 \gtrsim 10^{-11} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ . Abstraction reaction of  $\text{O}(^3\text{P})$  are normally very much slower than this and therefore a significant contribution by reaction (5) seems unlikely. Experimental tests showed that ppm concentrations of  $\text{O}_3$  and  $\text{HNO}_2$  do not react at a measurable rate over a period of hours.

In our preliminary report [3] it was suggested that the "excess"  $\text{NO}_2$  may result from the occurrence of the alternative photodissociation process:



followed by:





and reaction (4). For each dissociation by process (B), two molecules of  $\text{NO}_2$  are formed and one molecule of  $\text{NO}$  removed. The present data do not allow a rigorous test for the occurrence of process (B) but it is postulated in the absence of any reasonable alternative explanation of the unexpectedly high rates of  $\text{NO}_2$  formation.

Steady state analysis of the mechanism, comprising the two primary dissociation processes (A) and (B) and reactions (1) - (4) and (6), yields the following expressions for the rates of formation of  $\text{NO}$  and  $\text{NO}_2$ :

$$R_{\text{NO}} = [\text{HNO}_2] \left\{ (\Phi_A - \Phi_B)k_a - (\Phi_A + \Phi_B)k_a \left( \frac{k_1[\text{NO}]}{k_1[\text{NO}] + k_2[\text{NO}_2] + k_3[\text{HNO}_2]} \right) \right\} \quad (i)$$

$$R_{\text{NO}_2} = [\text{HNO}_2] \left\{ 2\Phi_B k_a + (\Phi_A + \Phi_B)k_a \left( \frac{k_3[\text{HNO}_2] - k_2[\text{NO}_2]}{k_1[\text{NO}] + k_2[\text{NO}_2] + k_3[\text{HNO}_2]} \right) \right\} \quad (ii)$$

where  $k_1$  and  $k_2$  are the effective bimolecular rate constants for reactions (1) and (2) with  $\text{M} = \text{N}_2 + \text{O}_2$  at 1 atm. and  $\Phi_A$  and  $\Phi_B$  are the quantum efficiencies for processes (A) and (B).  $k_a$  is the absorption rate per unit  $\text{HNO}_2$  concentration. These complex functions cannot be used for direct graphical test of the data but they may be simplified for certain limiting conditions, if the rate constants  $k_1$ ,  $k_2$  and  $k_3$  are of similar magnitude (see later). If the quantity  $k_x[\text{NO}_x]$  is substituted for  $(k_1[\text{NO}] + k_2[\text{NO}_2] + k_3[\text{HNO}_2])$  eqn. (i) becomes:

$$\frac{R_{\text{NO}}}{[\text{HNO}_2]} = (\Phi_A - \Phi_B)k_a - (\Phi_A + \Phi_B)k_a \frac{k_1[\text{NO}]}{k_x[\text{NO}_x]} \quad (iii)$$

For the limiting condition  $[\text{NO}] \rightarrow 0$ , and with a constant ratio  $[\text{NO}_2]/[\text{HNO}_2]$ , the slope of a plot of  $R_{\text{NO}}/[\text{HNO}_2]$  against  $[\text{NO}]/[\text{NO}_x]$  is equal to the quantity:

$$(\Phi_A + \Phi_B)k_a \left( \frac{k_1}{k_x(\text{NO} \rightarrow 0)} \right)$$

where  $k_x(\text{NO} \rightarrow 0)$  is the "mean" rate constant for the removal of OH by reactions (2) and (3). The intercept at  $[\text{NO}] = 0$  gives the quantity  $(\Phi_A - \Phi_B)k_a$ .

A plot of the experimental values according to eqn. (iii) for an approximately constant ratio  $[\text{NO}_2]/[\text{HNO}_2] = 0.08 (\pm 0.01)$  is shown in Fig. 3. The results for the two sets of experiments in which increasing amounts of  $\text{NO}$  were added to mixtures containing 0.8 ppm and 1.2 ppm  $\text{HNO}_2$  are seen to lie on the same curve. The curvature is ascribed to a change in the effective value of  $k_x$  as the relative proportion of  $\text{NO}$  in the mixture increases. The

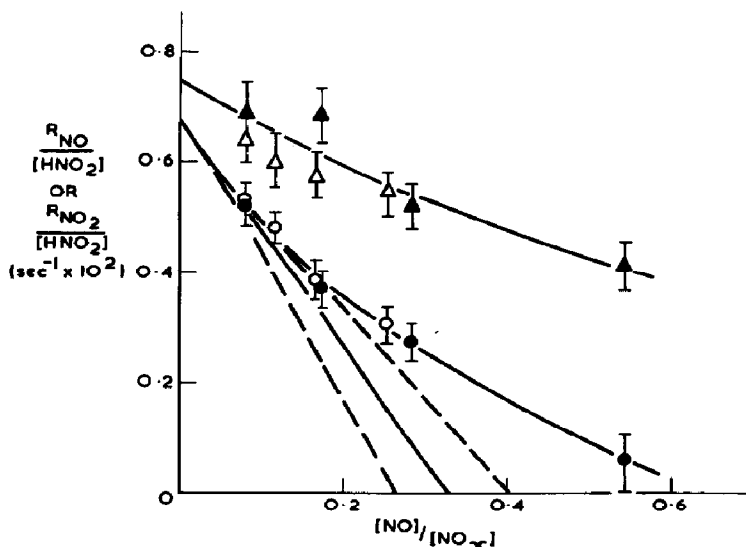


Fig. 3. Plot of  $R_{NO}/[HNO_2]$  (○, ●) and  $R_{NO_2}/[HNO_2]$  (△, ▲) against  $[NO]/[NO_x]$  ( $= NO + NO_2 + HNO_2$ ) in the photolysis of nitrous acid. Solid symbols = 0.8 ppm  $HNO_2$ ; open symbols = 1.25 ppm  $HNO_2$ .

values of the limiting slope ( $S$ ) and intercept ( $I$ ) at  $[NO] = 0$ , estimated graphically from this plot are  $S = 2.08 \pm 0.42 \times 10^{-2} s^{-1}$  and  $I = 0.68 \pm 0.02 \times 10^{-2} s^{-1}$  respectively.

If the quantity  $r = [NO_2]/[NO_x]$  then  $[HNO_2]/[NO_x] = 1-r$  for  $[NO] = 0$  and the following equations can be derived involving the limiting slope and intercept of the plot of eqn. (iii):

$$(\Phi_A + \Phi_B)k_a = S \left( \frac{k_2}{k_1} \right) r + \left( \frac{k_3}{k_1} \right) (1-r) \quad (iv)$$

$$(\Phi_A - \Phi_B)k_a = I \quad (v)$$

Equations (v)-(iv) gives:

$$-2\Phi_B k_a = I - S \left( \frac{k_2}{k_1} \right) r + \left( \frac{k_3}{k_1} \right) (1-r) \quad (vi)$$

An expression for  $2\Phi_B k_a$  may also be derived from eqn. (ii). When  $[NO] = 0$ , eqn. (ii) becomes:

$$I' = \quad (vii)$$

$$\frac{R_{NO_2}}{[HNO_2]} (NO \rightarrow 0) = 2\Phi_B k_a + (\Phi_A + \Phi_B)k_a \cdot \frac{k_1}{k_x} \left( \frac{k_3}{k_1} \frac{[HNO_2]}{[NO_x]} - \frac{k_2[NO_2]}{k_1[NO_x]} \right)$$

Since  $(\Phi_A + \Phi_B)k_a \times k_1/k_x = S$ , the following equation is obtained:

$$2\Phi_B k_a = I' - S \left( \frac{k_3}{k_1} (1-r) - \frac{k_2}{k_1} r \right) \quad (viii)$$

Figure 3 also shows the values of  $R_{\text{NO}_2}/[\text{HNO}_2]$  plotted against  $[\text{NO}]/[\text{NO}_x]$  for the experiments with added NO. A simple functional dependence of these variables is not expected but the plot may be used to derive a value of  $R_{\text{NO}_2}/[\text{HNO}_2]$  at  $[\text{NO}] = 0$  (i.e.  $I'$ ). The data show some scatter which reflects both the less accurate determination of  $R_{\text{NO}_2}$  (compared to  $R_{\text{NO}}$ ) and also the variations in  $[\text{NO}_2]/[\text{NO}_x]$  which can have a marked effect on  $R_{\text{NO}_2}/[\text{HNO}_2]$ . The estimated value of  $I'$  is  $0.75 \pm 0.05 \times 10^{-2} \text{ s}^{-1}$ .

From the values of  $I$ ,  $S$ ,  $I'$  and  $r$  eqns. (vi) and (viii) can be solved to obtain the ratio  $k_3/k_1$  i.e.

$$\frac{k_3}{k_1} = \frac{I' + I}{2S(1-r)} = 0.37$$

The uncertainty in this ratio is approximately  $\pm 20\%$  arising mainly from the uncertainty in  $S$ .

In order to calculate the dissociation rates  $\Phi_A k_a$  and  $\Phi_B k_a$  a knowledge of the ratio  $k_2/k_1$  is necessary. From our preliminary study of the photolysis of  $\text{HNO}_2$  it was estimated that  $k_2/k_1 \approx 1.0 \pm 0.2$  [3]. No other experimental determinations of this ratio at 1 atm. pressure and 300 K seem to have been reported, although estimates have been made at higher temperatures. In studies of the reaction of  $\text{NO}_2$  with  $\text{H}_2$  Rosser and Wise [5] concluded that reactions (1) and (2) had "essentially equal" rate constants at 600 - 700 K with  $\text{M} = \text{H}_2$ . From a study of the thermal reaction between  $\text{H}_2\text{O}_2$  and  $\text{NO}$ , Asquith [6] found  $k_2/k_1 = 1.0 \pm 0.5$  at 550 K and 100 Torr pressure. Maximum and minimum limits for the ratio at 1 atm. and 300 K can be estimated from recent measurements of the absolute rate constants of reactions (1) and (2) at lower pressures. On the basis of low pressure data [up to 30 Torr for reaction (1) and 300 Torr for reaction (2)], Morley and Smith [7] estimate high pressure limiting values of  $k_1 = 1.7 \times 10^{-10}$  and  $k_2 = 1.2 \times 10^{-11} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  (i.e. for the bimolecular reactions  $\text{OH} + \text{NO}_x = \text{HNO}_x$ ). The value of  $k_1 = 1.1 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ , calculated from the third order rate constant determined for reaction (1) with  $\text{M} = 30 \text{ Torr } \text{H}_2$  [7] gives a lower limit for this rate constant at 1 atm. Combining these data with those of Simoniatis and Heicklen [8] for the indirect determination of  $k_2 = 5 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  for  $\text{M} = 1 \text{ atm. } \text{N}_2$  at 300 K, it can be concluded that:  $0.1 < k_2/k_1 < 5$ . Table 2 shows the values of  $\Phi_A k_a$  and  $\Phi_B k_a$  calculated from eqns. (v) and (vi) using the values of  $k_2/k_1 = 1, 0.1$  and 5. It will be seen that the choice of  $k_2/k_1$  within these limits does not influence  $\Phi_A k_a$  greatly but can make an appreciable difference to the derived value of  $\Phi_B k_a$ .

With a knowledge of the ratios  $k_3/k_1$  and  $k_2/k_1$ , it is possible to calculate values of  $\Phi_A k_a$  and  $\Phi_B k_a$  from all of the experimental data in Table 1. If  $k_3/k_1 = 0.37$  and  $k_2/k_1 = 1$ , the following equations may be derived from eqns. (i) and (ii):

$$\frac{R_{\text{NO}}}{[\text{HNO}_2]} = \Phi_A k_a (1 - X) - \Phi_B k_a (1 + X) \quad (\text{ix})$$

TABLE 2

Primary dissociation rates in the photolysis of  $\text{HNO}_2$ 

$k_2/k_1$ assumed value	Dissociation rates ( $\text{s}^{-1} \times 10^{-2}$ )*	
	$\Phi_A k_a$	$\Phi_B k_a$
0.1	0.728	0.023
1.0	0.775	0.091
5.0	0.991	0.308

\*Calculated for  $I = 0.68 \times 10^{-2} \text{ s}^{-1}$ ,  $I' = 0.750 \times 10^{-2} \text{ s}^{-1}$ ,  $S = 2.08 \times 10^{-2} \text{ s}^{-1}$ ; see text.

$$\frac{R_{\text{NO}_2}}{[\text{HNO}_2]} = \Phi_A k_a \cdot Y + \Phi_B k_a (2 + Y) \quad (\text{x})$$

where

$$X = \frac{[\text{NO}]}{[\text{NO}] + [\text{NO}_2] + 0.37[\text{HNO}_2]}$$

$$\text{and } Y = \frac{0.37[\text{HNO}_2] - [\text{NO}_2]}{[\text{NO}] + [\text{NO}_2] + 0.37[\text{HNO}_2]}$$

Solution of these simultaneous equations gives  $\Phi_A k_a$  and  $\Phi_B k_a$  from the measured  $R_{\text{NO}}$  and  $R_{\text{NO}_2}$  values in a given mixture of  $\text{HNO}_2$ ,  $\text{NO}$  and  $\text{NO}_2$ . The dissociation rates are, of course, subject to the uncertainty in  $k_2/k_1$ .

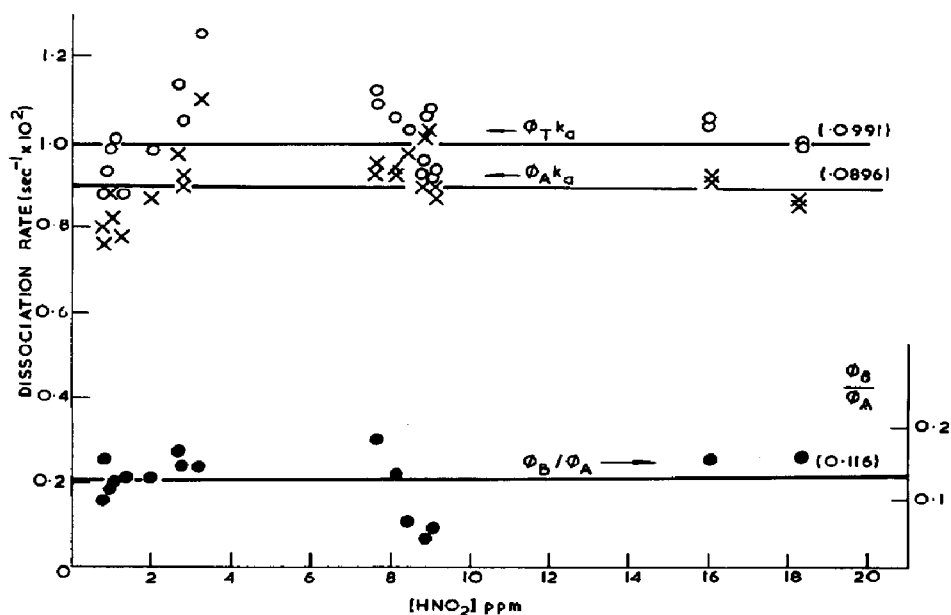


Fig. 4. Calculated values of the total primary dissociation rate,  $\Phi_T k_a$ , the dissociation rate  $\Phi_A k_a$  and the ratio  $\Phi_B/\Phi_A$  plotted against the concentration of nitrous acid. Mean values given in parentheses.

Figure 4 shows a plot of the quantities  $\Phi_A k_a$ ,  $\Phi_T k_a$  [ $= (\Phi_A + \Phi_B) k_a$ , the total photodissociation rate] and  $\Phi_B/\Phi_A$  as a function of the concentration of  $\text{HNO}_2$ . The values of  $\Phi_A k_a$  showed considerable variation but there was no significant trend over the 20 fold change in  $\text{HNO}_2$  concentration. The variations are ascribed mainly to fluctuations in the light intensity. The ratio  $\Phi_B/\Phi_A$  also showed no overall trend with  $\text{HNO}_2$  concentration but some of the values in the middle of the concentration range were significantly less than the mean value of 0.116. These differences are rather greater than expected from the estimated experimental error which possibly suggests that the mechanism involving process (B) is incorrect. However, we cannot find any reasonable alternative description of the average behaviour of the system at the present time. Some support for the mechanism and numerical values for the rate parameters adopted comes from the consistency in the  $\Phi_A$  and  $\Phi_B$  values, calculated by eqns. (ix) and (x), for the results at high  $[\text{NO}]/[\text{NO}_x]$  (see Table 3).

TABLE 3

Calculated values of  $\Phi_A k_a$  and  $\Phi_B k_a$  from experiments with added NO

$\text{HNO}_2$	$\frac{\text{NO}}{\text{NO}_x}$	$(\text{s}^{-1} \times 10^2)$	
		$\Phi_A k_a^*$	$\Phi_B k_a^*$
0.83	0.080	0.756	0.113
1.31	0.080	0.773	0.096
1.29	0.115	0.803	0.088
1.25	0.167	0.768	0.105
0.81	0.172	0.811	0.130
1.19	0.253	0.841	0.113
0.79	0.280	0.780	0.086
0.77	0.540	0.960	0.111

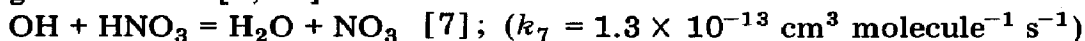
\*Calculated using  $k_3/k_1 = 0.37$  and  $k_2/k_1 = 1.0$ .

It is of interest to compare the dissociation rate,  $\Phi_T k_a$ , with the estimated absorption rate of  $\text{HNO}_2$  in the photolysis cell. The latter may be derived from the measured absorption rate of  $\text{NO}_2$  ( $k'_a = 2.8 \times 10^{-2} \text{ s}^{-1}$ ) and a consideration of the extinction coefficients  $\epsilon_{\text{NO}_2}$  and  $\epsilon_{\text{HNO}_2}$  in the wavelength region 330 - 380 nm. The average value of  $\epsilon_{\text{NO}_2}$  in this region is close to  $145 \text{ l mol}^{-1} \text{ cm}^{-1}$  [9]. The absorption spectrum of  $\text{HNO}_2$  shows a diffuse structure in this region [4] and evaluation of  $\epsilon_{\text{HNO}_2}$  from the available data is difficult. Asquith and Tyler [10] have estimated that  $\epsilon_{\text{HNO}_2}$  lies between 50 and  $150 \text{ l mol}^{-1} \text{ cm}^{-1}$  at 368 nm (the maximum absorption in this region). The average  $\epsilon_{\text{HNO}_2}$  for the range 340 - 380 nm is estimated to be roughly one-half the maximum and therefore  $\epsilon_{\text{HNO}_2} \approx 50 \pm 25 \text{ l mol}^{-1} \text{ cm}^{-1}$ . Thus for weak absorption by both gases :

$$k_a(\text{HNO}_2) = k'_a(\text{NO}_2) \times \frac{50(\pm 25)}{145} = 0.97 \pm 0.45 \times 10^{-2} \text{ s}^{-1}$$

The average value of  $\Phi_T k_a$  was  $0.991 \times 10^{-2} \text{ s}^{-1}$  and therefore  $0.7 < \Phi_T < 1.9$ . When the uncertainties are taken into account it is probable that the quantum yield for  $\text{HNO}_2$  dissociation is close to unity. If  $\Phi_T = 1$ , it follows that  $\Phi_A \approx 0.9$  and  $\Phi_B \approx 0.1$  (assuming that  $k_2/k_1 \approx 1$ ). It is concluded, therefore, that the predominant process following absorption by nitrous acid in the near u.v is dissociation to give  $\text{OH} + \text{NO}$ . A small fraction ( $\sim 10\%$ ) of the  $\text{HNO}_2$  molecules appear to undergo dissociation to give  $\text{H} + \text{NO}_2$  but more evidence is required to confirm this result. A study of the photolysis of nitrous acid using selected wavelengths above and below the energy threshold for H atom production would provide useful information on this matter.

The experimental value of the rate constant ratio  $k_3/k_1$  ( $= 0.37 \pm 0.06$ ) shows that the rate of abstraction of an H atom from  $\text{HNO}_2$  is of the same magnitude as the addition of OH to NO and  $\text{NO}_2$  (if  $k_2 \approx k_1$ ) at 1 atm. pressure. If  $k_1 \approx k_2 = 5 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ ,  $k_6 = 1.8 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ , which is more than an order of magnitude faster than the analogous reaction [7, 11]:



If the reactions have similar pre-exponential factors, reaction (3) must have a considerably lower activation energy than reaction (7). A possible explanation of this arises from the unusual properties of the *cis* rotational isomer of  $\text{HNO}_2$ , which exists in equilibrium with the more stable *trans* isomer with  $[\text{trans-HNO}_2] \approx 2.5[\text{cis-HNO}_2]$  at 300 K. It has been shown [12] that the H-O bond is unusually long and possesses a low vibrational frequency compared with other simple polyatomic molecules such as  $\text{H}_2\text{O}$ ,  $\text{HCOOH}$ ,  $\text{HNO}_3$ , *trans-HNO*<sub>2</sub>, etc. On this basis the abstraction of an H atom from *cis-HNO*<sub>2</sub> might be expected to have a lower activation energy than from  $\text{HNO}_3$ .

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